

# **Advanced Numerical and Experimental Transient Modelling of Water and Gas Pipeline Flows Incorporating Distributed and Local Effects**

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July 2008

## APPENDIX A

# TRANSFER FUNCTION OF UNSTEADY FRICTION FOR TRANSIENT LAMINAR FLOW

Unsteady wall shear stress for transient laminar pipe flow is expressed as a function of  $\partial\hat{V}/\partial t(s)$  in the Laplace domain with a transfer function  $\hat{\phi}(s)$  [Zielke, 1968].

$$\hat{\tau}_o(s) = \hat{\phi}(s) \frac{\partial\hat{V}}{\partial t}(s) \quad \text{where} \quad \hat{\phi}(s) = \frac{\rho R_p}{\zeta_1 \left( i \sqrt{\frac{s}{\nu}} R_p \right) - 2} = \frac{\rho R_p}{i \sqrt{\frac{s}{\nu}} R_p \frac{J_0(i \sqrt{\frac{s}{\nu}} R_p)}{J_1(i \sqrt{\frac{s}{\nu}} R_p)} - 2} \quad (\text{A.1})$$

where the circumflex accent represents the Laplace transform of time variable,  $\tau_o$  is the shear stress at the pipe wall,  $s$  is the Laplace variable,  $V$  is the mean velocity of fluid,  $\rho$  is the density of fluid,  $R_p$  is the radius of pipe,  $i$  is the unit imaginary number,  $\nu$  is the kinematic viscosity,  $J_0$  is the Bessel function of first kind and zero order,  $J_1$  is the Bessel function of the first kind and first order,  $\zeta_1$  is the modified quotient of Bessel function of the first order defined as  $\zeta_1(z) = z \cdot J_0(z) / J_1(z)$ , and  $z$  is a complex number.

The inverse Laplace transform of Eq. A.1 is described as the inverse Laplace form  $\phi(u)$  of  $\hat{\phi}(s)$  and its convolution with the rate of change of velocity and with the time  $u$  in the convolution integral.

$$\tau_o(t) = \int_0^t \phi(u) \frac{\partial V}{\partial t}(t-u) du \tag{A.2}$$

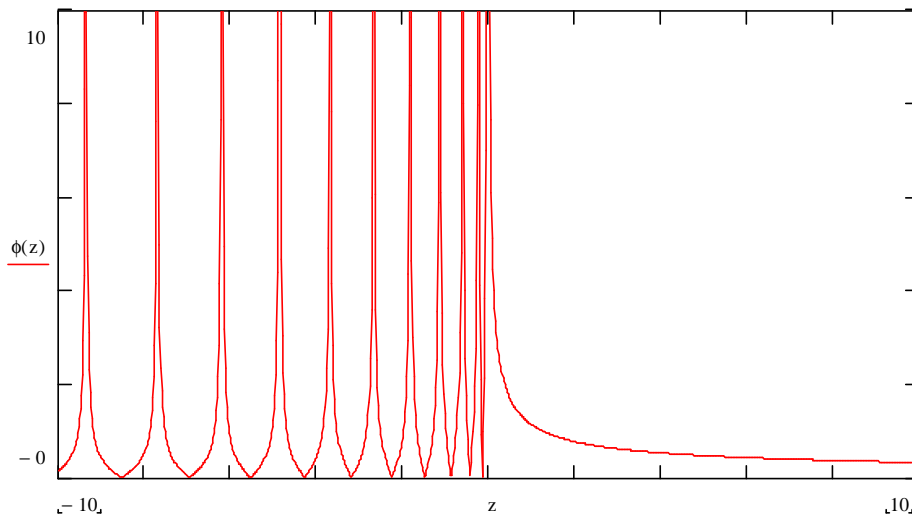
To find the Laplace inversion of the transfer function, the complex inversion formula can be used

$$\phi(t) = \lim_{\omega \rightarrow \infty} \frac{1}{2\pi i} \int_{\sigma-i\omega}^{\sigma+i\omega} \hat{\phi}(s) e^{st} ds \tag{A.3}$$

where  $\omega$  is the angular frequency. This complex inversion formula can be evaluated by using the residue theorem that is a powerful tool to evaluate path integrals of an analytic function over a closed curve.

$$\phi(t) = \frac{1}{2\pi i} \oint_C \hat{\phi}(s) e^{st} ds = \sum_{j=1}^k \text{Res} [\hat{\phi}(s) e^{st}, s_j] \tag{A.4}$$

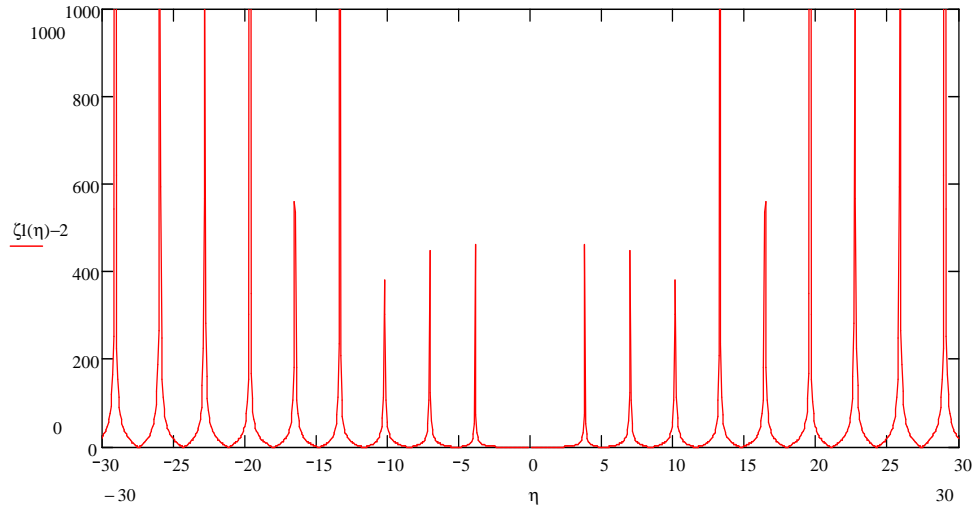
The transfer function (analytic function) is holomorphic (differentiable everywhere within some open space) on all open subsets of the complex plane except a set of isolated points, which are poles for the function as shown in Fig. A.1.



**Figure A.1 Absolute Value of Transfer Function on the Complex Plane**

The poles occur at the  $\tau_o$  of the denominator (DE) of the transfer function. The first root is  $s = 0$  and an infinite number of root is  $s_j = -\eta_j^2 \cdot \nu / R_p^2$ . The constants  $\eta_j$  are

obtained by the evaluating of  $\zeta_1(\eta) - 2 = 0$  as shown in Fig. A.2 and Table A.1. The interval between them is approaching  $\pi$ .



**Figure A.2** Roots of the Equation,  $\zeta_1(\eta) - 2 = 0$

**Table A.1** The First 20 Roots of the Equation,  $\zeta_1(\eta) - 2 = 0$

$j$	$\eta_j$	$j$	$\eta_j$
1	5.13562	11	36.86286
2	8.41724	12	40.00845
3	11.61984	13	43.15345
4	14.79595	14	46.29800
5	17.95982	15	49.44216
6	21.11700	16	52.58602
7	24.27011	17	55.72963
8	27.42057	18	58.87302
9	30.56920	19	62.01622
10	33.71652	20	65.15927

The function  $\phi(t)$  is given by the sum of all residues of  $\hat{\phi}(s)e^{st}$

$$\text{Res} [\hat{\phi}(s)e^{st}, s_j] = \frac{\rho R_p}{\frac{\partial \zeta_1}{\partial s}(\eta_j)} e^{s_j t} \tag{A.5}$$

Differentiation of  $\zeta_1$  yields

$$\frac{\partial \zeta_1}{\partial s}(\eta_j) = \frac{R_p^2}{2\nu} \quad (\text{A.6})$$

which is constant for all residues except the one at the origin. Therefore

$$\mathbf{Res} [\hat{\phi}(s)e^{st}, s_j] = \frac{2\nu\rho}{R_p} e^{-\frac{\eta_j^2}{R_p^2}\nu t} \quad (\text{A.7})$$

By using Eq. A.4,

$$\phi(\tau) = \frac{4\nu\rho}{R_p} + \frac{2\nu\rho}{R_p} \sum_{j=1}^{\infty} e^{-\eta_j^2 \tau} \quad (\text{A.8})$$

where the dimensionless time is,  $\tau = \nu t / R_p^2$ .

Finally, the unsteady wall shear stress is expressed by

$$\tau_o(t) = \frac{2\rho\nu}{R_p} \int_0^t \frac{\partial V}{\partial t}(u) W(t-u) du \quad (\text{A.9})$$

where  $W(\tau) = e^{-\eta_1^2 \tau} + e^{-\eta_2^2 \tau} + e^{-\eta_3^2 \tau} + \dots$  that is a function of the dimensionless time  $\tau$ . The equation for energy loss by unsteady friction is

$$h_{uf}(t) = \frac{16\nu}{gD^2} \int_0^t \frac{\partial V}{\partial t}(u) W(t-u) du \quad (\text{A.10})$$

Eq. A.10 can be easily calculated by the first-order approximation in MOC or FDM (including a conservative solution scheme).

## APPENDIX B

# TRANSFER FUNCTION OF UNSTEADY FRICTION FOR TRANSIENT TURBULENT FLOW

Unsteady wall shear stress for transient turbulent pipe flow is expressed as a function of  $\partial\hat{V}/\partial t(s)$  in the Laplace domain with a transfer function  $\hat{\Phi}(s)$  [Vardy and Brown, 2003].

$$\frac{\hat{\tau}_o(s)}{\rho v_w} = \frac{\hat{\Phi}(s)}{s} \frac{\partial\hat{V}}{\partial t}(s) \quad (\text{B.1})$$

They idealized the flow distribution by two different viscous regions. One is annular region of width  $b$  ( $b = 0.2 \times \text{pipe radius } (R_p)$ ) adjacent to the wall where the viscosity is assumed to vary linearly from  $\nu_w$  at the wall to  $\nu_c$  at the interface between the annulus and an inner core region. Another is the core region where the viscosity is assumed to be uniform and equal to  $\nu_c$ .  $\hat{\Phi}(s)$  is a transfer function between the transforms of the mean velocity and the unsteady component of the wall shear stress. It satisfies

$$\hat{\Phi}(s) = \sqrt{s/v_w} \cdot \left[ \begin{array}{l} C_1(s) \cdot I_1 \left( \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \\ - C_2(s) \cdot K_1 \left( \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \end{array} \right] \cdot G(s) \quad (\text{B.2})$$

$$- 1 / ((v_c - v_w) / (b \cdot v_w) \cdot v_w)$$

$$\cdot (1 - v_c / v_w - (v_c - v_w) / (b \cdot v_w)) \cdot (R_p - b) / 2 \cdot G_s$$

where

$$\frac{1}{G(s)} = ((R_p - b) + 0.5b) \cdot \frac{(v_c - v_w) / (b \cdot v_w) \cdot v_w}{R_p^2 \cdot s}$$

$$\left[ \begin{array}{l} \left( \begin{array}{l} C_1(s) \cdot \sqrt{v_c / v_w \cdot 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \\ \cdot I_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \\ - C_2(s) \cdot \sqrt{v_c / v_w \cdot 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \\ \cdot K_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \\ - v_c / v_w \cdot 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2 / 2 \end{array} \right) \\ \cdot \left( \begin{array}{l} C_1(s) \cdot \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \\ \cdot I_1 \left( \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \\ - C_2(s) \cdot \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \\ \cdot K_1 \left( \sqrt{4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2} \right) \\ - 4 \cdot s / v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2 / 2 \end{array} \right) \end{array} \right] \quad (\text{B.3a})$$

$$+ \frac{1}{R_p^2} \left[ \begin{array}{l} 2 \cdot (R_p - b) \cdot \sqrt{v_c / s} \cdot (1 + H(s)) \\ \cdot \frac{I_1((R_p - b) \cdot \sqrt{s / v_c})}{I_0((R_p - b) \cdot \sqrt{s / v_c})} - (R_p - b)^2 \end{array} \right]$$

$$\frac{1}{G_s} = -\frac{2((R_p - b) + b/2)}{R_p^2 \cdot ((v_c - v_w)/(b \cdot v_w))^2 \cdot v_w} \cdot \left[ \left( \frac{(R_p - b)}{2} + \frac{v_c/v_w}{(v_c - v_w)/(b \cdot v_w)} \right) \cdot (v_c/v_w \cdot \ln(v_c/v_w) - v_c/v_w + 1) - \frac{(v_c - v_w)/(b \cdot v_w) \cdot b^2}{2} \right] - \frac{(R_p - b)^2}{R_p^2 \cdot ((v_c - v_w)/(b \cdot v_w))^2 \cdot v_w} \quad (\text{B.3b})$$

$$C_1(s) = -1/ \left[ \frac{\left( \frac{((v_c - v_w)/(b \cdot v_w))^2 \cdot (R_p - b)^2}{8 \cdot v_c/v_w} + \ln(v_c/v_w) \cdot \left( \frac{(v_c - v_w)/(b \cdot v_w) \cdot (R_p - b)}{2} + v_c/v_w - \frac{v_c/v_w - 1}{\ln(v_c/v_w)} \right) \right)}{I_0\left(\sqrt{4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right)} \cdot K_0\left(\sqrt{v_c/v_w \cdot 4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right) - K_0\left(\sqrt{4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right) \cdot I_0\left(\sqrt{v_c/v_w \cdot 4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right) \right] \cdot \left[ K_0\left(\sqrt{4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right) \cdot (1 + H(s)) - K_0\left(\sqrt{v_c/v_w \cdot 4 \cdot s/v_w \cdot ((v_c - v_w)/(b \cdot v_w))^2}\right) \right] \quad (\text{B.3c})$$



$$C_2(s) = -1/ \left[ \begin{array}{l} I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right] \quad (B.3d)$$

$$\cdot \left[ \begin{array}{l} I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \cdot (1 + H(s)) \end{array} \right]$$

$$H(s) = - \frac{I_1 \left( (R_p - b) \cdot \sqrt{s / v_c} \right) / I_0 \left( (R_p - b) \cdot \sqrt{s / v_c} \right) + A_3(s) \cdot I_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) - A_4(s) \cdot K_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right)}{I_1 \left( (R_p - b) \cdot \sqrt{s / v_c} \right) / I_0 \left( (R_p - b) \cdot \sqrt{s / v_c} \right) + A_5(s) \cdot I_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) - A_6(s) \cdot K_1 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right)} \quad (B.3e)$$

$$A_3(s) = -1/ \left[ \begin{array}{l} I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right] \quad (B.3f)$$

$$\cdot \left[ \begin{array}{l} K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right]$$

$$A_4(s) = -1/ \left[ \begin{array}{l} I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right] \quad (B.3g)$$

$$\left[ \begin{array}{l} I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right]$$

$$A_5(s) = -1/ \left[ \begin{array}{l} I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right] \quad (B.3h)$$

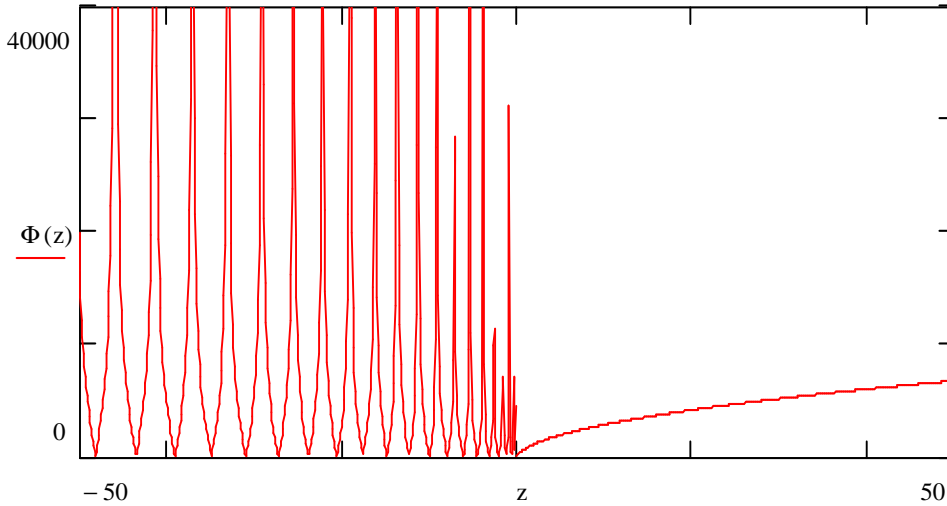
$$\cdot K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right)$$

$$A_6(s) = 1/ \left[ \begin{array}{l} I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot K_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ - K_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \\ \cdot I_0 \left( \sqrt{v_c / v_w \cdot 4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right) \end{array} \right] \quad (B.3i)$$

$$\cdot I_0 \left( \sqrt{4 \cdot s / (v_w \cdot ((v_c - v_w) / (b \cdot v_w))^2)} \right)$$

where  $s$  is the Laplace transform variable,  $I_n$  is the modified Bessel function of the first kind and  $n$ th order,  $K_n$  is the modified Bessel function of second kind and  $n$ th order,  $G(s)$  is the function relating the driving force and the mean velocity, and  $G_s$  is the steady flow equivalent of  $G(s)$ .

Similar to the transfer function of unsteady wall shear stress for transient laminar pipe flow, the transfer function of unsteady wall shear stress for transient turbulent pipe flow, Eq. B.2 with Eq. B.3a to B.3i, shows the set of isolated points that are poles for the function as shown in Fig. B.1.



**Figure B.1 Absolute Value of the Transfer Function on the Complex Plane**

Although the inverse Laplace transformation of transfer function for laminar flow can be performed analytically to obtain an exact expression for the weighting function, there is no analytical solution to find inverse Laplace transform of Eq. B.2 because of the complexity of the equation. Vardy and Brown [2003] proposed a different approach by approximating the weighting function. The following part shows the procedure of the approximation.

The inverse Laplace transform of Eq. B.1 also can be expressed as a convolution based on the weighting function derived for unsteady laminar flow in the time domain.

$$\tau_o(t) = \frac{2\rho v_{lam}}{R_p} \int_0^T W \frac{\partial V}{\partial t} dt^* \quad (\text{B.4})$$

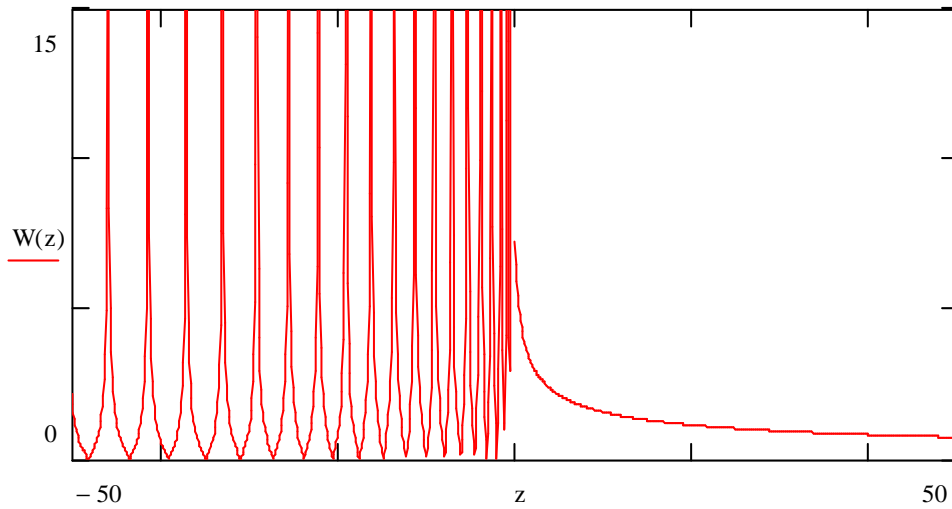
where  $T$  is the elapsed time since the beginning of the unsteadiness,  $t^* = T - t$  is backward-measured time from the instant at which the integral is being evaluated,  $v_{lam}$  is the laminar kinematic viscosity, the weighting function  $W$  is a function of  $t^*$  whereas the acceleration  $\partial V/\partial t$  is a function of  $t$ . The Laplace transform of Eq. B.4 is

$$\hat{\tau}_o(t) = \frac{2\rho\nu_{lam}}{R_p} \hat{W}(s) \frac{\partial \hat{V}}{\partial t}(s) \quad (B.5)$$

By comparison with Eq. B.1, the transformed weighting function is

$$\hat{W}(s) = \frac{R_p}{2} \frac{\nu_w}{\nu_{lam}} \frac{\hat{\Phi}(s)}{s} \quad (B.6)$$

Fig. B.2 shows the absolute value of the transformed weighting function on the complex plane.



**Figure B.2 Absolute Value of Weighting Function on the Complex Plane**

The transformed weighting function is approximated by a simple function that is possible for application of an inverse Laplace transformation.

$$\hat{W}_{app}(s) = \frac{A}{\sqrt{s+B}} \quad (B.7)$$

where  $A$  and  $B$  is the coefficients for the approximated weighting function and the subscript  $app$  represent the approximation of weighting function.

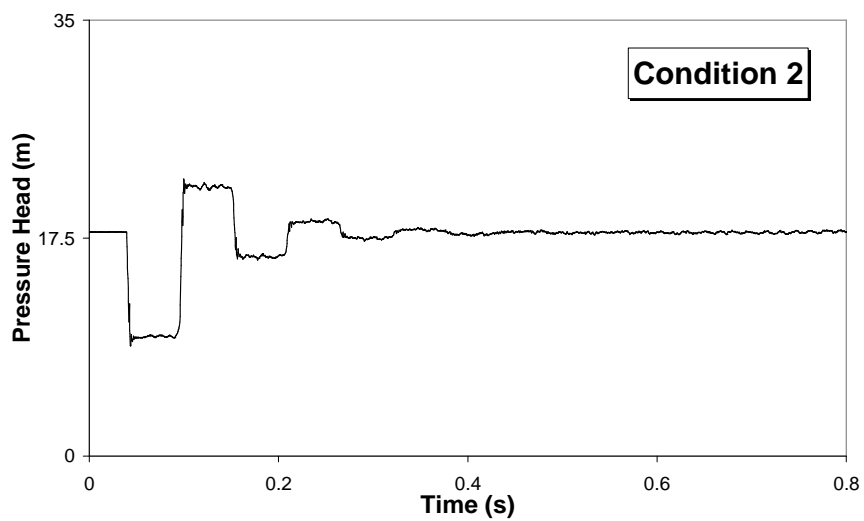
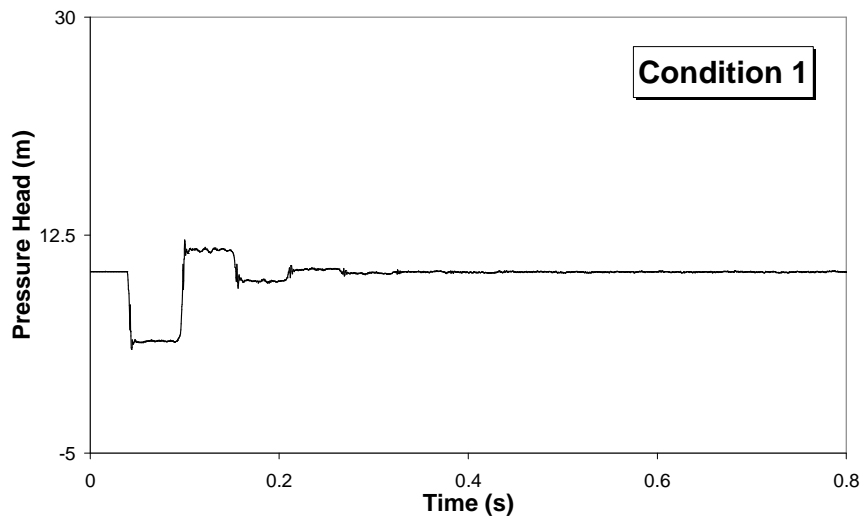
The inverse Laplace transform of the approximated weighting function, Eq. B.7, is

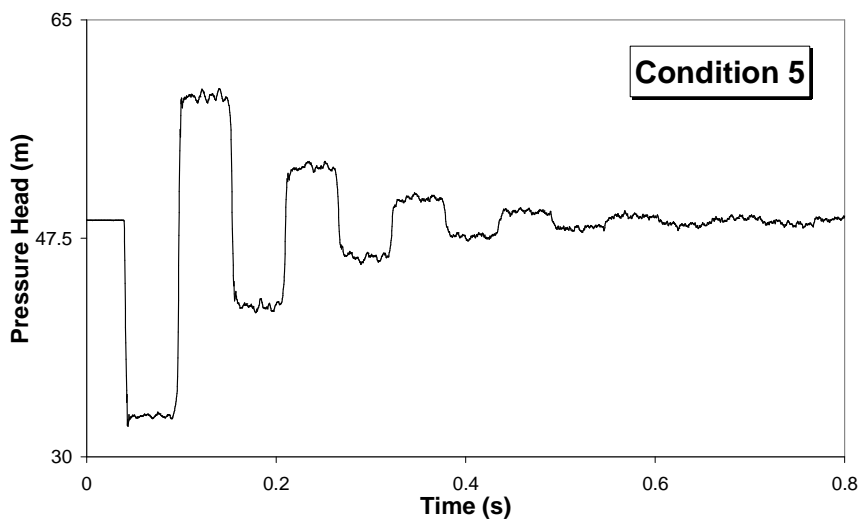
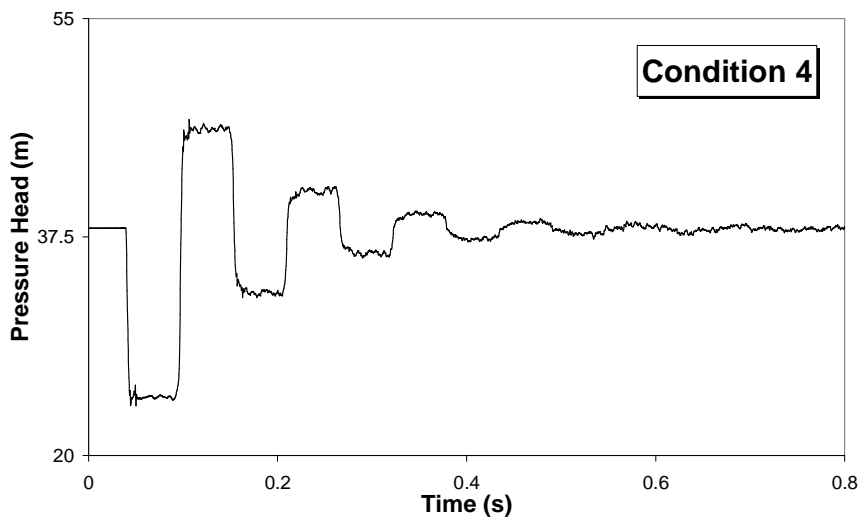
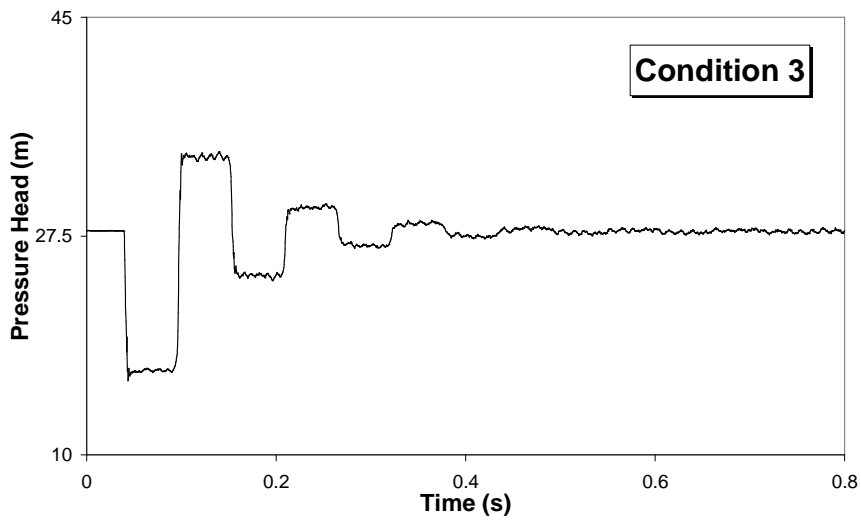
$$W_{app}(\tau) = \frac{A^* e^{-B^* \tau}}{\sqrt{\tau}} \quad (\text{B.8})$$

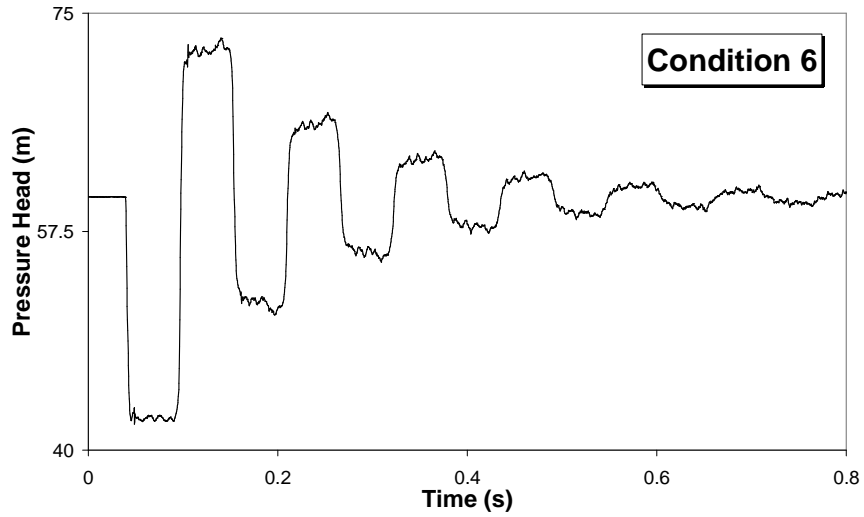
This is the weighting function of the unsteady shear stress for transient turbulent pipe flow in the time domain. The weighting functions are defined in terms of the dimensionless time  $\tau = 4v_{lam}t / D^2$ .  $A^*$  and  $B^*$  are the coefficients for the weighting function. The values of these coefficients are determined by matching the asymptotic states of Eq. B.6 and Eq. B.7 at large and very small Laplace transform variables.

# APPENDIX C

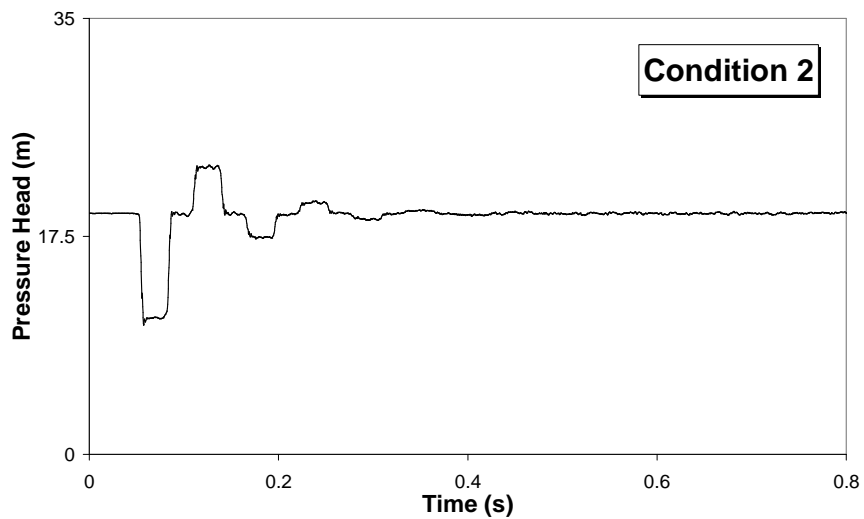
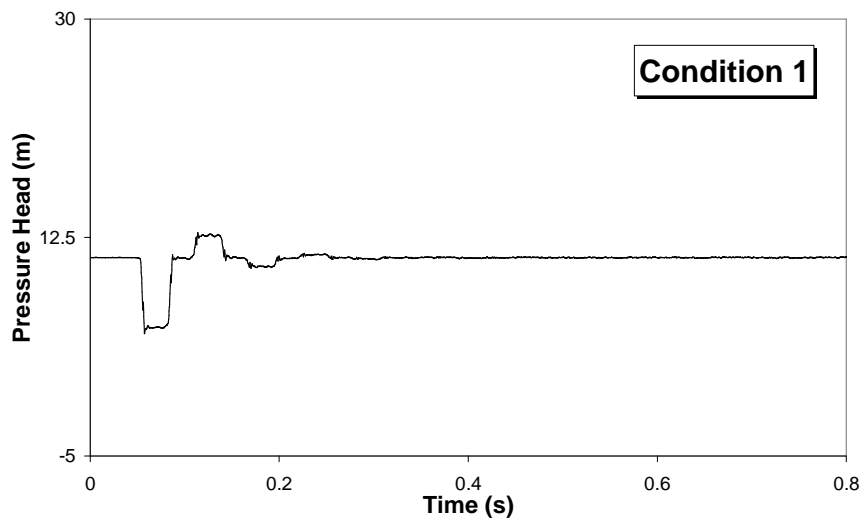
## MEASURED TRANSIENT DATA BY A FAST VALVE OPENING EVENT



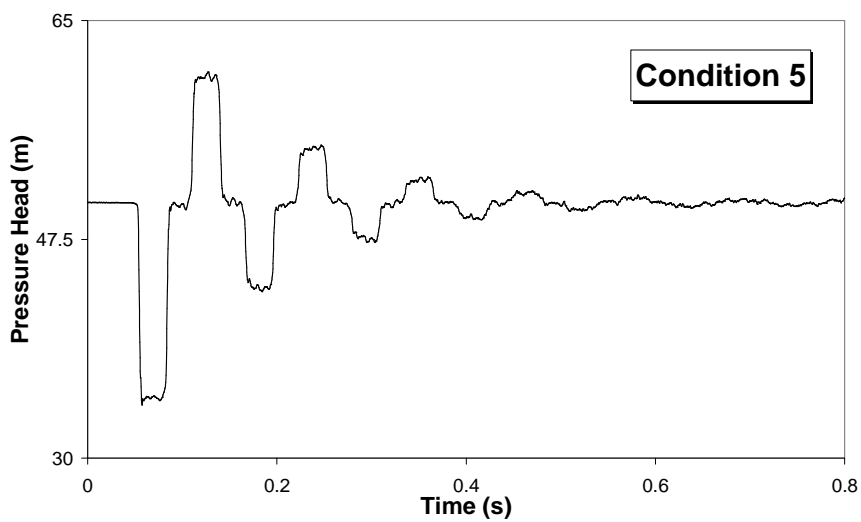
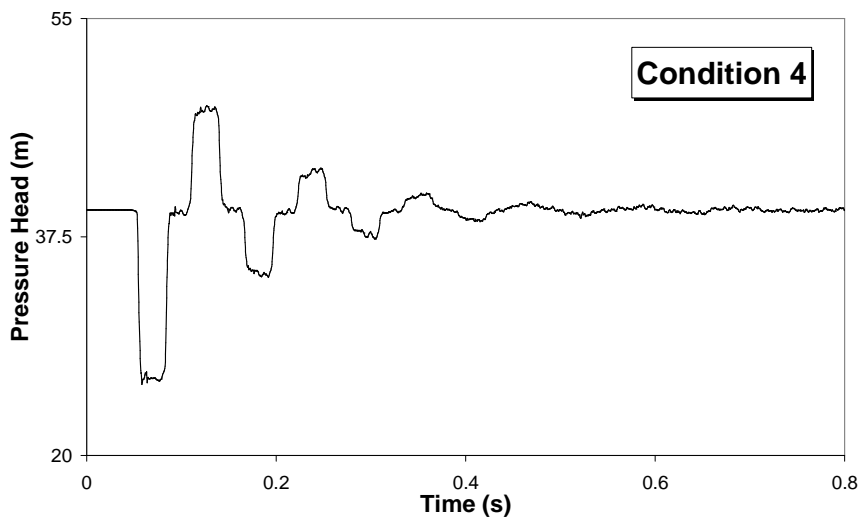
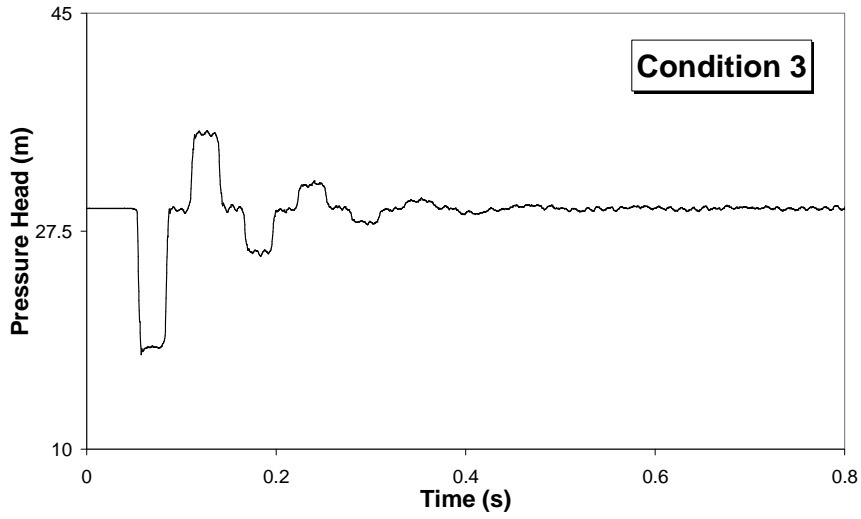


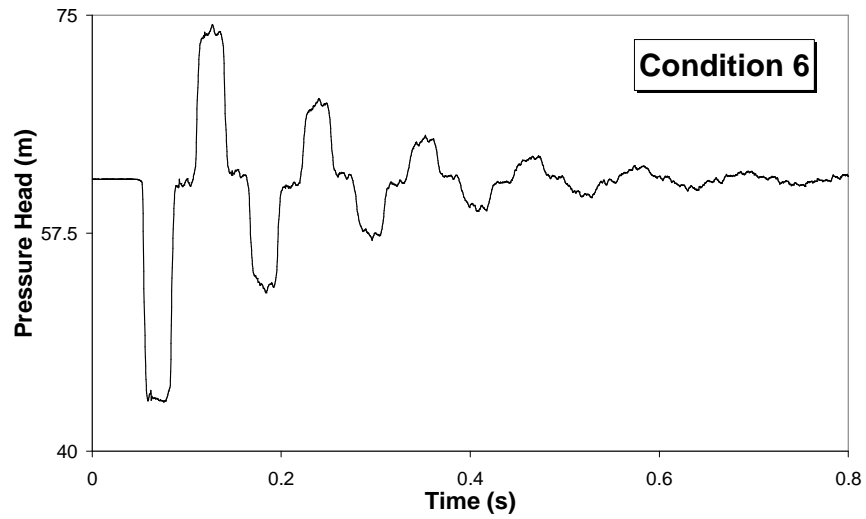


**Figure C.1 Measured Transient Data at the Downstream End  
(Flow conditions are shown in Table 5.4)**









**Figure C.2 Measured Transient Data at the Middle of Pipe  
(Flow conditions are shown in Table 5.4)**



# APPENDIX D

## THE EFFECT OF JOINTS ON TRANSIENT PIPE FLOWS

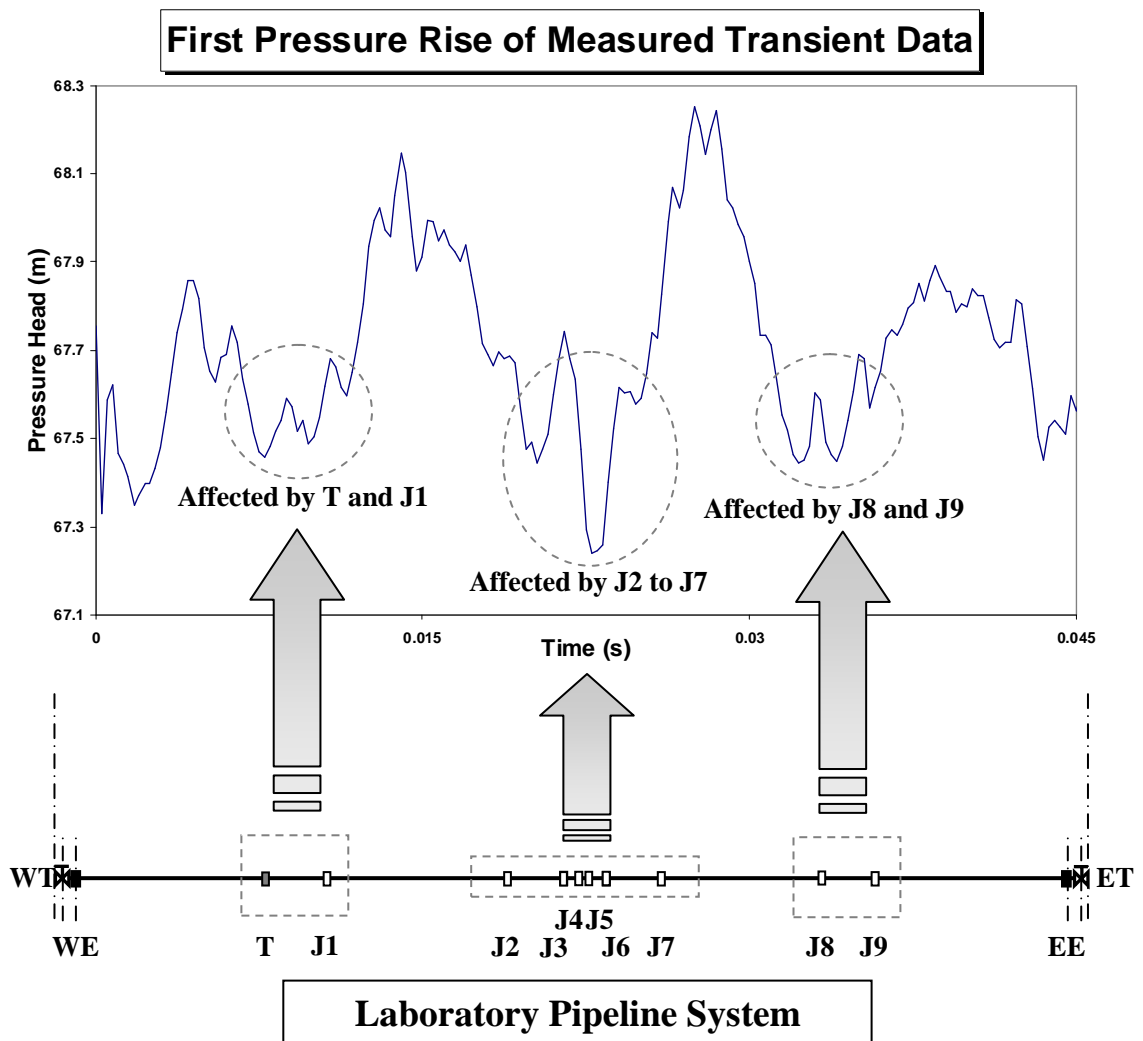


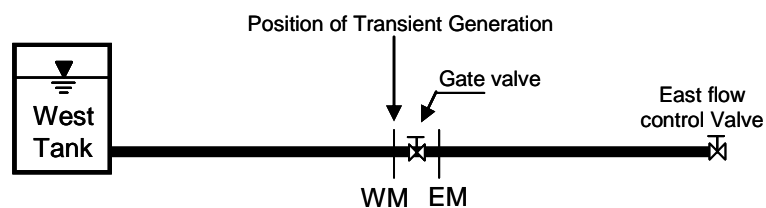
Figure D.1 Effect of Pipe Joints During Transients



## APPENDIX E

# THE EFFECT OF A VALVE ON TRANSIENT PIPE FLOWS

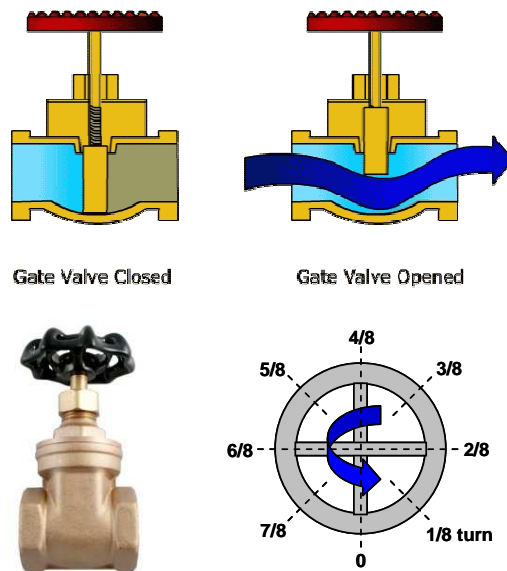
Laboratory experiments have been executed for the investigation of the effect of a gate valve during transient events. The experimental apparatus described in Chapter 4 is used. The gate valve as shown in Fig. E.2 is inserted between J4 and J5. Transients are generated at the middle of pipe (WM) by a side-discharge solenoid valve with a fast operating time after closing the east flow control valve. The sampling frequency of measured data is 4 kHz and the water temperature is 23°C. Fig. E.1 shows the pipe system layout for gate valve tests.



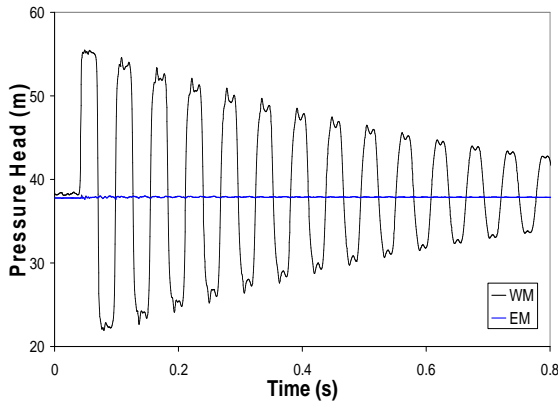
**Figure E.1 Pipeline System Layout**

The pressure data are collected according to the degree of valve opening or closure by adjusting the hand-wheel of the gate valve as shown in Fig. E.2. The fully open valve position is approximately 9 turns ( $9 \times 360^\circ$ ) from the fully closed valve condition. Fig. E.3 shows the measured data. The measured data present the state of transmission and reflection waves by the gate valve. When the gate valve is fully closed, the measured data at the WM shows full transients as a single pipeline composed of west tank, pipeline from

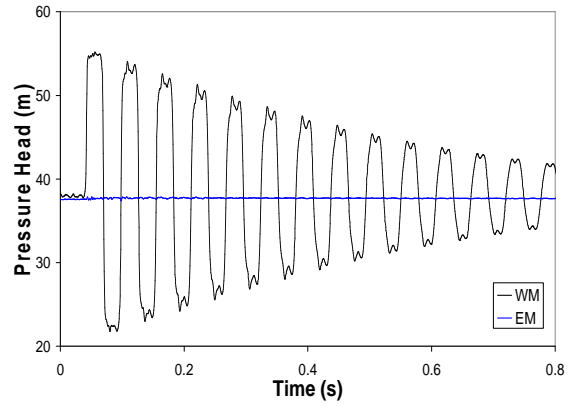
west tank to gate valve, and downstream end valve, but the measured data at the EM has no propagation of pressure waves because the fully closed gate valve completely isolates the right-hand part of the gate valve. The situation is similar for valve openings of 1/8 and 2/8 turn opening. When the gate valve is opened to 3/8 opening of the hand-wheel, the pressure waves are very slightly propagated into the right-hand part of the system across the gate valve. The measured data of WM shows a large pressure damping when comparing the Fig. E.3 (a) to (c) but there is no wave reflection from the gate valve. This case is very special because the right-hand pipe of the gate valve can be regarded as a lumped capacitance that severely reduces the pressure wave. From the 4/8 turn open position (Fig. E.3 (e)), as the opening area of the gate valve increases the reflection of pressure wave by the gate valve decreases and the transmission of pressure wave through the gate valve increases. Finally, the measured data of 1 turn open are almost identical with the data of fully open, although the opening area is very small when considering the area of the fully opened condition. It may be noticed that the pressure wave can be easily or fully propagated through a small opening area. Condition assessment for valves uses these kinds of transient data to analyse the dynamic characteristics of valves.



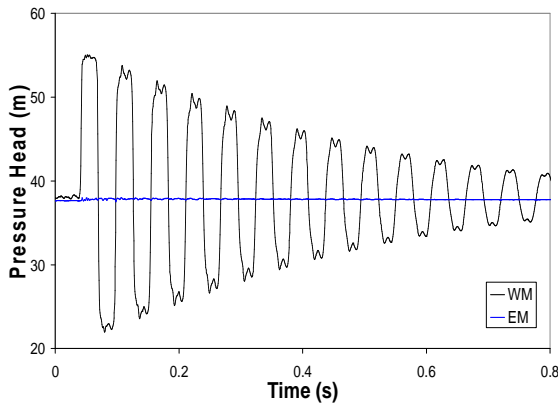
**Figure E.2 Gate Valve**



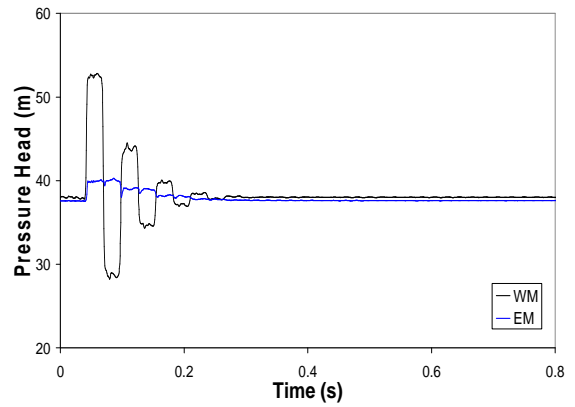
**(a) Fully closed**



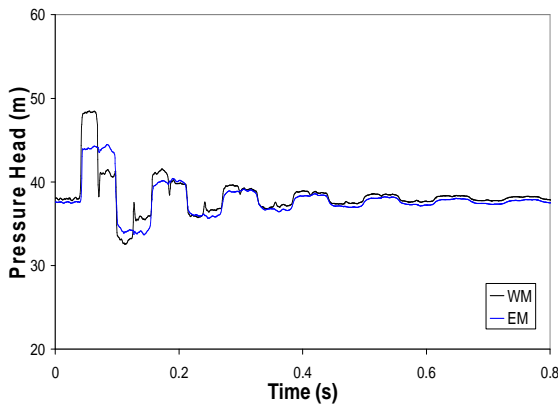
**(b) 1/8 Turn Open**



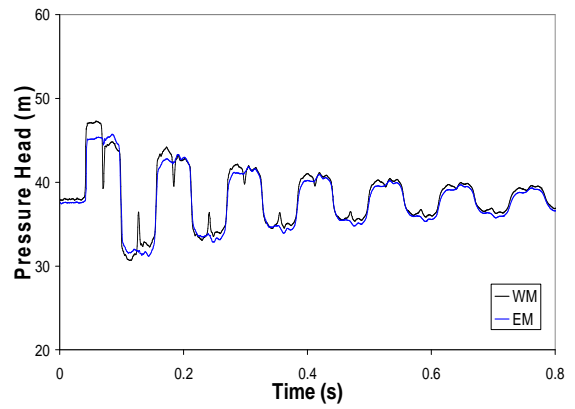
**(c) 2/8 Turn Open**



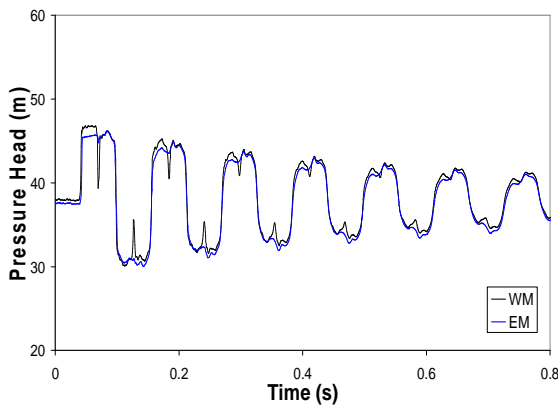
**(d) 3/8 Turn Open**



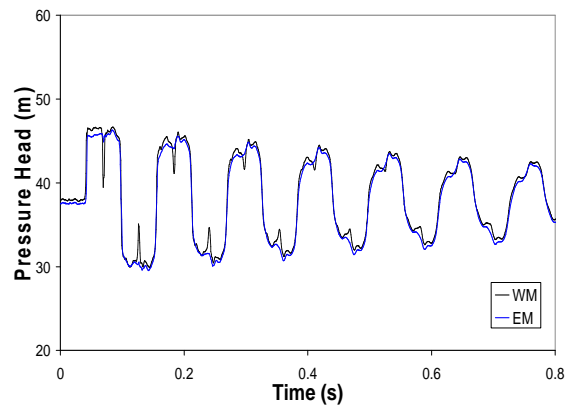
**(e) 4/8 Turn Open**



**(f) 5/8 Turn Open**



**(g) 6/8 Turn Open**



**(h) 7/8 Turn Open**



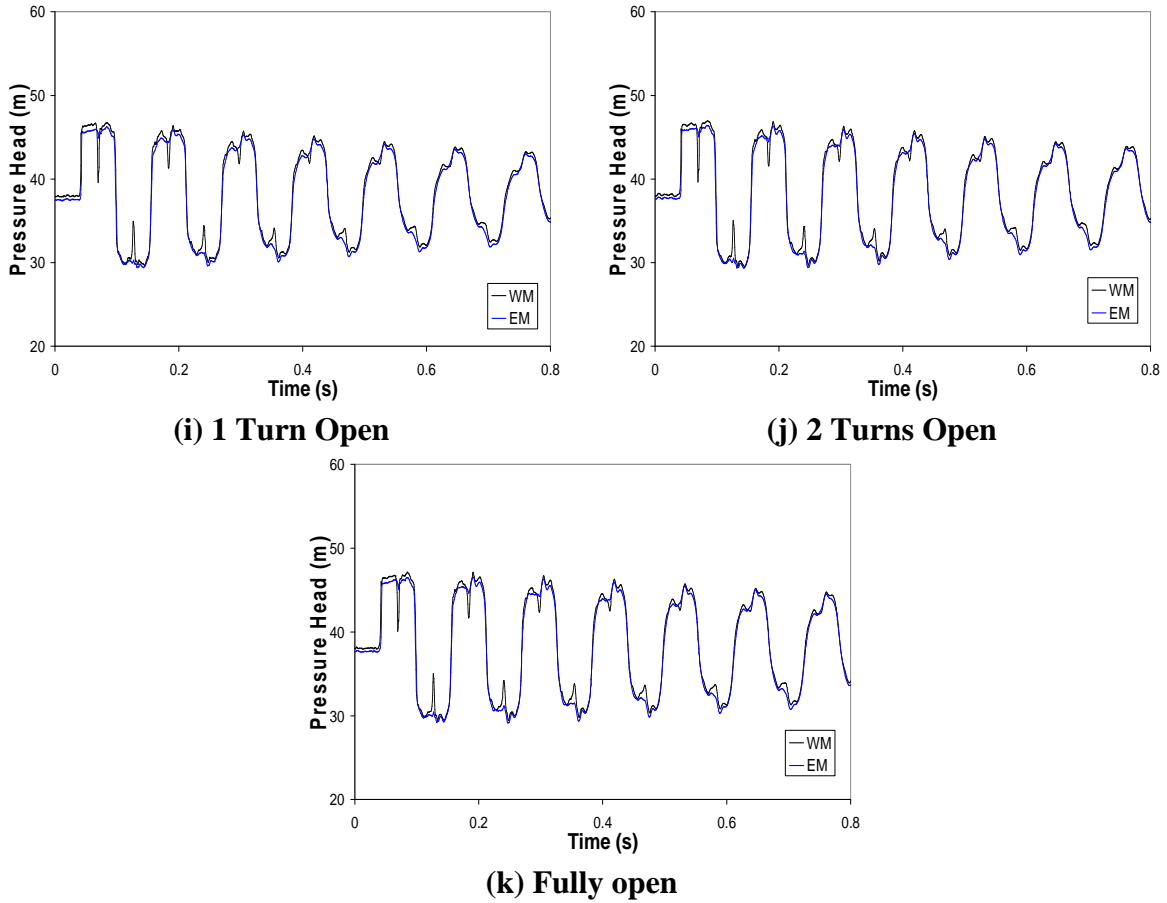
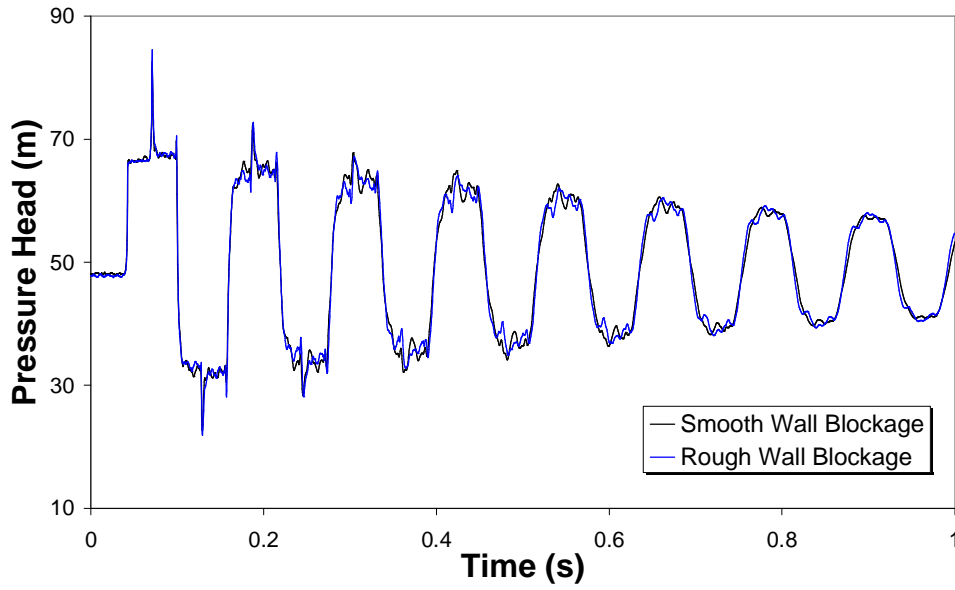


Figure E.3 Measured Data according to the Degree of Valve Open

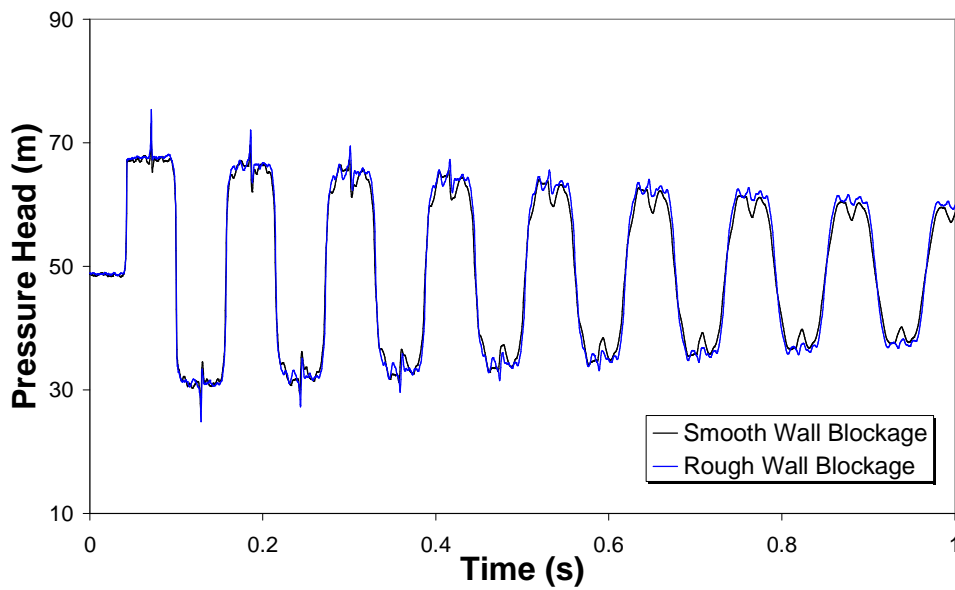
## APPENDIX F

# **THE EFFECT OF ROUGH WALL BLOCKAGES ON TRANSIENT PIPE FLOWS**

Natural blockages formed by solid deposition or pipe wall corrosion have large roughness height and irregular shape when compared to the pipe wall material. For the natural blockage tests during transients, the surfaces of brass blockages presented in Chapter 8 were artificially cut by a large drill bit to make coarse screw thread on the inside surface of blockage. Fig. F.1 and F.2 shows the comparison of measured transient data between smooth wall blockages used in Chapter 8 and rough wall blockages with a 1 mm screw thread for 5 mm bore blockage and with 2 mm screw thread for 10 mm bore blockage. All blockages have a 153 mm axial length and are installed at the middle of pipeline. Transients are generated at the WE by a side-discharge solenoid valve and pressure waves are also measured at the WE. The results of blockages with rough wall are almost same as the results of blockages with smooth wall. The dominant physical phenomena of blockages still seem to be the eddy inertia effect of the turbulent jet flow because the length of blockage may be too short to affect the transient pressure wave.



**Figure F.1 Comparison between Measured Data with Smooth Wall Blockage (5 mm Blockage Bore) and with Rough Wall Blockage (5 mm Blockage Bore and 1 mm Roughness Height by Screw Thread)**



**Figure F.2 Comparison between Measured Data with Smooth Wall Blockage (10 mm Blockage Bore) and with Rough Wall Blockage (10 mm Blockage Bore and 2 mm Roughness Height by Screw Thread)**

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